

ME-318 Engineering Heat Transfer

Chapter 7 Important Concepts & Equations

- Thermal Boundary Layer Thickness, Laminar flow:

$$\frac{\delta}{\delta_T} \approx \text{Pr}^{1/3}$$

- Laminar Local and Average Nusselt Numbers:

$$Nu(x) = \frac{hx}{k_f} = 0.332 (\text{Re}_x)^{1/2} (\text{Pr})^{1/3}$$

$$\text{Pr} \geq 0.6$$

$$\overline{Nu}_L = \frac{\bar{h} L}{k_f} = 0.664 (\text{Re}_L)^{1/2} (\text{Pr})^{1/3}$$

$$\overline{Nu}_L = 2Nu(x)$$

- Turbulent Boundary Layers:

$$\frac{\delta}{\delta_T} \approx 1$$

$$Nu(x) = 0.0296 (\text{Re}_x)^{4/5} (\text{Pr})^{1/3} \quad 0.6 \leq \text{Pr} \leq 60$$

Turbulent over entire plate

$$\overline{Nu}_L = 0.037 \text{Re}_L^{4/5} \text{Pr}^{1/3}$$

Mixed Flow

$$\overline{Nu}_L = \left(0.037 \text{Re}_L^{4/5} - 871 \right) \text{Pr}^{1/3}$$

- Cross Flow Over Cylindrical Tube:

$$\overline{Nu}_L = \frac{\bar{h} D}{k_f} = 0.3 + \frac{0.62(\text{Re}_D)^{1/2} \text{Pr}^{1/3}}{\left[1 + (0.4/\text{Pr})^{2/3} \right]^{1/4}} \left[1 + \left(\frac{\text{Re}_D}{282,000} \right)^{5/8} \right]^{4/5}$$