Exam 2 – Key – v. 1.5 (Ave 55, High 72, Low 20 (⊗)) BE-382, Winter '08-'09, Dr. C. S. Tritt

1. (30) In an attempt to reduce the overall pressure drop in a 20.0 m long, 1.00 cm diameter cooling water line, a 16.0 m long segment in the middle of the line is replaced with a 2.00 cm diameter tube. Estimate and compare the pressure drops in these two configurations. The volumetric flow rate is 2.00×10^{-4} m³/s (which is equivalent to 12.0 liters/min). The density of the water is 1,002 kg/m³ and viscosity is 1.00×10^{-3} kg/(m·s) (which is equal to 1.00 cp). Assume smooth surfaces, fully developed flow and an energy correction factor, α , of 1.00.

1. Common values (given)

$$V = 2.00 \times 10^{-4} \text{ m}^3/\text{s}$$

 $e = 1,002 \text{ Kg/m}^3$
 $M = 1.00 \times 10^{-3} \text{ Kg/m} \text{ s}$
 $D = 1.00 \text{ cm}$
Case A O
 K
 $L = 20 \text{ m}$
 $D = 2.00 \text{ cm}$
 W
 $L = 16 \text{ m}$
 M

$$D(m) = 0.01 = 0.02$$

$$A = \frac{\pi D^2}{4} (m^2) 7.85 \times 10^{-5} = 3.14 \times 10^{-4}$$

$$V = \frac{V}{4} (m_8) = 2.55 = 0.637$$

$$N_{Re} = \frac{e V D}{4} (hone) = 25,500 = 12,800$$

$$f (from chart) = 0.026 = 0.028$$

"Minor Losses"
Expansion
$$K_{L,z} = d \left(1 - \frac{d^2}{D^2}\right)^2 = \left(\frac{3}{4}\right)^2 = 0.562$$

Contraction $K_{L,z} = 0.400$ (at $\frac{d^2}{D^2}$ of 0.25)

$$\begin{aligned} & AP_{P,pes} = \int \frac{L}{D} \frac{e^{V^2}}{2} \quad \mathcal{H}_{PTS} \\ & AP_{L} = K_{L} \frac{e^{V^2}}{2} \quad \mathcal{H}_{PTS} \\ & AP_{IT} \quad for the two Cases; \\ & Case I; \quad D = 1.00 \text{ cm}, \quad L = 20 \text{ m} \\ & AP_{I} = 1.69 \times 10^{5} Pa = \frac{169 \text{ KPa}}{-6 \text{ pr}} \quad \text{i0 prs} \\ & AP_{I} = 1.69 \times 10^{5} Pa = \frac{169 \text{ KPa}}{-6 \text{ pr}} \quad \text{i0 prs} \\ & Case 2: \quad D = 2.00 \text{ cm}, \quad L = 16 \text{ m} + \frac{10 \text{ prs}}{-6 \text{ pr}} \quad \text{frot} \\ & D = 1.00 \text{ cm}, \quad L = 4 \text{ m} + \frac{10 \text{ prs}}{-6 \text{ pr}} \quad \text{frot} \\ & Sudden \quad \text{Expansion} + \frac{1}{5} \text{ sudden} \quad \text{Expansion} + \frac{1}{5} \text{ sudden} \quad \text{Case} 12 \text{ prs} \\ & AP = 4.55 \times 10^{3} + 3.39 \times 10^{4} + 1.83 \times 10^{3} + 1.30 \times 10^{3} \\ & = 4.16 \times 10^{4} \text{ Pa} = 41.6 \text{ KPa} \quad 12 \text{ prs} \\ & So, \quad \text{the pressure drop is fess in} \\ & Case 2. \end{aligned}$$

2. (35) International rules state that ping-pong (table tennis) balls shall weigh 2.7 grams and be 40 millimeters in diameter. What is the terminal velocity of a ping-pong ball at sea level where $\mu_{air} = 1.82 \times 10^{-5} \text{ kg/(m·s)}$, $\rho_{air} = 1.20 \text{ kg/m}^3$ and $g = 9.81 \text{ m/s}^2$? Neglect buoyancy (I assume it's accounted for in the specified weight of the ball). Without doing any calculations, would a solid depleted uranium ($\rho = 19.1 \text{ g/cm}^3$) ball of the same diameter have a higher or lower terminal velocity under the same conditions?

1. Common values (given)

$$\dot{V} = 2.00 \times 10^{-4} \text{ m}^{3}\text{s}$$
 Assume $\alpha = 1$
 $e = 1,002 \text{ Kg/m}^{3}$
 $M = 1.00 \times 10^{-3} \text{ Kg/m}.\text{s}$
 $D = 1.00 \text{ cm}$
Case A
 $case B$
 d
 $D = 1.00 \text{ cm}$
 $D = 2.00 \text{ cm}$
 $k = L = 16 \text{ m}^{-3}$
Values in segments
 $D(m)$
 $A = \frac{\pi}{4} D^{2} (m^{2}) 7.85 \times 10^{-5}$
 $A = \frac{\pi}{4} D^{2} (m^{2}) 2.55$
 $O.637$
 $N_{\text{Re}} = \frac{e \nu D}{4} (n_{\text{max}})$
 $25,500$
 $12,800$
 $f (from chart)$
 $O.026$
 0.028
"Minor Losses"
Expansion $K_{L,e} = 0.400$ (at $\frac{d^{2}}{D^{2}} d 0.25$)

Iteration

Guess V (m/s)	NRe	CD	Fp
1	2630	0.4	3.01×10-4
10	26,300	0.4	3.01 × 10-2
9,0	23,700	0.4	2.44 × 10-2

At this point, I Know $9.0 < v < 10 \frac{10}{5}$ In general, I could Keep guessing Until I found the answer. However, In this case CD is not changing, So just solve $F_g = \frac{Ae}{2} C_0 V^2$ for V to get:

Depleted uranium would have a higher terminal velocity because the same drag equations would apply but Fg would be much greater.

For depleted Uranium, I get V = 332 mg Co off by 10x -2 Not showing calc. of Npe => Cp -8 Using Stoke's Law - not checking result -20 3. (35) Cross out terms on the given differential balance equations and provide boundary and initial conditions as needed to solve for the steady state velocity distribution in the fully developed flow of an incompressible fluid in a square duct with dimensions 2W wide by 2H high. Align the direction of flow with the z-axis of your coordinate system. Some credit will be given for choosing the best origin for your coordinate system.

Continuity -

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} + \frac{\partial u_z}{\partial z} = 0$$

Rectangular (Cartesian) Coordinates -

$$x \operatorname{direction}^{z} \left(\frac{\partial v_{x}}{\partial t} + v_{x} \frac{\partial v_{x}}{\partial x} + v_{y} \frac{\partial v_{x}}{\partial y} + v_{z} \frac{\partial v_{x}}{\partial z} \right)^{2} = \frac{\partial p}{\partial x} + \mu \left[\frac{\partial^{2} v_{x}}{\partial x^{2}} + \frac{\partial^{2} v_{x}}{\partial y^{2}} + \frac{\partial^{2} v_{z}}{\partial z^{2}} \right] + \rho g_{x}$$

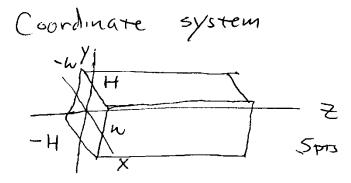
y direction

$$\rho\left(\frac{\partial v_y}{\partial t} + v_x\frac{\partial v_y}{\partial x} + v_y\frac{\partial v_y}{\partial y} + v_z\frac{\partial v_y}{\partial z}\right) = -\frac{\partial p}{\partial y} + \mu\left[\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2}\right] + \rho g_y$$

$$z \operatorname{direction}_{p\left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z}\right)}^2 = -\frac{\partial p}{\partial z} + \mu \left[\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2}\right] + \rho g_z$$

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B.C's

No
$$\begin{cases} Uz = U_x = U_y = 0 & x = W = -W \\ U_z = U_x = U_y = 0 & y = H + -H \\ \\ Sym. \\ \frac{\partial Uz}{\partial x} = 0 & x = 0 \\ \frac{\partial Uz}{\partial y} = 0 & y = 0 \\ U_x = 0 & x = 0 \\ U_y = 0 & y = 0 \\ \end{cases}$$

Incompressible implies $\boldsymbol{\rho}$ is constant so used incompressible version of continuity.